

# SPREADSHEET PROCEDURE FOR SIMULATING SETPOINT TRACKING IN SISO BY DYNAMIC MATRIX CONTROL

LARRY K. JANG AND ROGER C. LO  
*California State University • Long Beach, CA 90840-5103*

The objective of this work is to present a spreadsheet tool that illustrates an ideal case of dynamic matrix control (DMC) calculations. The ideal case presented in this work is a hypothetical single-input-single-output DMC control system for setpoint tracking, in the absence of disturbance and mismatch between the measured and predicted process variable, at various move suppression coefficients. Students in an undergraduate process control class who followed the procedure to build the spreadsheet would gain a good basic understanding of DMC.

## A BRIEF OUTLINE OF DYNAMIC MATRIX CONTROL METHOD

### Dynamic matrix: prediction of future process response based on present and future control moves

Industry has widely accepted control strategies based on model predictive control (MPC), primarily in multiple-input-multiple-output processes. The first known industrial application of linear MPC was known as dynamic matrix control (DMC). Initially, DMC was introduced for the single-input-single-output (SISO) cases.<sup>[1]</sup> The development of DMC and its recent status has been reported in the literature.<sup>[2]</sup>

Moving horizon control is a key feature of dynamic matrix

control. This type of controller employs a model internal to the controller architecture to predict the process variable for  $n_p$  steps into the future based on control moves for  $n_p$  steps in the past. The future process response predicted from the past control moves is called “free response.”<sup>[3]</sup> Then, the algorithm calculates the predicted error (setpoint–free response, with model mismatch and disturbance taken into consideration) for future  $n_p$  steps, followed by an optimization scheme to calculate the present and future control moves needed to minimize or suppress the net error (predicted error–future

*Larry K. Jang is professor of chemical engineering at California State University, Long Beach. He earned his B.S. and M.S. from National Taiwan University and Ph.D. from University of Southern California, all in chemical engineering. His area of research in recent years is remote automatic control using LabVIEW technology.*

*Roger C. Lo is an assistant professor in the Department of Chemical Engineering at California State University, Long Beach. He received his Ph.D. in chemical engineering from Texas A&M University. Roger teaches undergraduate and graduate required courses (fluids, engineering mathematics, and transport phenomena) and also numerical analysis using Excel and MATLAB for chemical engineering calculations. Roger's research interest focuses on microfluidics and its applications at the interface of biology, chemistry, and engineering, such as microreactors, miniaturized high-throughput chemical/biological assays, and portable instruments for environmental analysis and monitoring.*

process response due to the present and future control moves). Once the computation is done, only the first calculated control move is implemented and the algorithm moves one time step ahead. The free response is predicted and new control moves are calculated again for this new time step. The procedure of predicting the future free response, calculating the present and future control moves to suppress error, and implementing the first calculated control move is carried out as time moves on.

The first crucial step in implementing DMC in a SISO case is to obtain information about how the process responds to a step change in the controller output. This procedure is very much like the traditional approach of finding the dynamic model of a process by making a step change in the controller output (in the manual mode) and observing the response of the process variable, followed by fitting the response curve to the model chosen (such as the first-order-plus-dead-time (FOPDT) model). With the model parameters (such as process gain, first-order time constant, and dead time), an engineer may use well-established tuning rules, such as Ziegler-Nichols method, Cohen-Coon method, and Internal Model Control (IMC) method, to find appropriate tuning parameters for a proportional-integral-derivative (PID) feedback controller. However, instead of fitting response data to a particular model, the DMC method calculates the coefficients of the system's step response model (SRM).<sup>[1]</sup>

Assuming that the system is initially at steady state and the initial value of the process variable is 0, the coefficient can be defined as follows:

$$\text{Coefficient of SRM} = a_i = \frac{y(t_i)}{\Delta u(t_0)} \quad (1)$$

where  $\Delta u(t_0)$  is the magnitude of step change made (and held constant) in the controller output at  $t = t_0$  and  $y(t_i)$  is the response of the process variable at  $t = t_i$ . We may consider the  $t_i$ 's as discrete times of choice and/or sampling times. In DMC applications, at least 10 discrete time steps are needed between  $t_0$  and  $t_{ss}$  (time to reach the next steady state). The number of time steps taken to reach steady state is called *model horizon* (denoted as  $m$  in this work). If the controller output changes from the previous value by the magnitudes of  $\Delta u(t_0), \Delta u(t_1), \dots, \Delta u(t_{n_c-1})$ , at present and future times ( $t = t_0, t_1, \dots, t_{n_c-1}$ ) and held constant thereafter, we may predict the response of the process at any future time  $t_i$  ( $i = 1, 2, \dots, n_p$ ) by the principle of superposition. The effect of a control move made at  $t_0$  would take  $t_i$  time steps to reach  $t_i$ . Likewise, the effect of a control move made at  $t_1$  would take  $t_{i-1}$  steps to reach  $t_i$ , and so forth. Since the effect is additive, we have Eq. (2).

$$y(t_i) = a_1 \Delta u(t_0) + a_{i-1} \Delta u(t_1) + \dots \text{(for } n_c \text{ terms)}, \quad (2)$$

Assuming that one is making 12 steps of prediction ahead (*i.e.*, the *prediction horizon*  $n_p = 12$ ) based on the subsequent control moves for 5 steps (at  $t_0, t_1, t_2, t_3$ , and  $t_4$ ) and held con-

stant thereafter (*i.e.*, the control horizon  $n_c = 5$ ), Eq. (2) may be rewritten in the matrix form [Eqs. (3) and (4)]:

$$\begin{bmatrix} y(t_1) \\ y(t_2) \\ y(t_3) \\ \vdots \\ y(t_{12}) \end{bmatrix} = \begin{bmatrix} a_1 & 0 & 0 & 0 & 0 \\ a_2 & a_1 & 0 & 0 & 0 \\ a_3 & a_2 & a_1 & 0 & 0 \\ \vdots & \vdots & \vdots & \vdots & \vdots \\ a_{11} & a_{10} & a_9 & a_8 & a_7 \\ a_{12} & a_{11} & a_{10} & a_9 & a_8 \end{bmatrix} \begin{bmatrix} \Delta u(t_0) \\ \Delta u(t_1) \\ \Delta u(t_2) \\ \Delta u(t_3) \\ \Delta u(t_4) \end{bmatrix} \quad (3)$$

$$[y]_{12 \times 1} = [A]_{12 \times 5} [\Delta u \text{ (present and future)}]_{5 \times 1} \quad (4)$$

The first term on the right-hand side of Eqs. (3) and (4) ( $[A]_{12 \times 5}$ ) is called the dynamic matrix. Note that the present and future control moves  $\Delta u(t_0), \dots, \Delta u(t_4)$  are not known *a priori*. We need to use the procedure below to calculate them.

### FREE RESPONSE: PREDICTION FOR FUTURE PROCESS RESPONSE BASED ON PAST CONTROL MOVES

Free response is defined as the predicted process response for  $t > t_0$  (at  $t_1, t_2, \dots, t_{n_p}$ ) based on the past control moves ( $\Delta u(t_{-n_p}), \Delta u(t_{-n_p+1}), \dots, \Delta u(t_{-1})$ ) if no further controller outputs are changed at  $t_0, t_1, t_2, \dots$ . The effect of the control move made at  $t_{-1}$  would take 2 steps to reach  $t_1$ , 3 steps to reach  $t_2$ , ..., and so forth. Likewise, the effect of the control move made at  $t_{-2}$  would take 3 steps to reach  $t_1$ , 4 steps to reach  $t_2, \dots$ , and so forth. Therefore, for a system in which  $n_p = 12$ , we would obtain the prediction vector  $[y_p]_{12 \times 1}$  for the free response (due to past control moves only) as

$$\begin{bmatrix} y_p(t_1) \\ y_p(t_2) \\ \vdots \\ y_p(t_{12}) \end{bmatrix} = \begin{bmatrix} y(t_{-12}) \\ y(t_{-11}) \\ \vdots \\ y(t_{-1}) \end{bmatrix} + \begin{bmatrix} a_{13} & \dots & a_3 & a_2 \\ a_{14} & \dots & a_4 & a_3 \\ \vdots & \dots & \vdots & \vdots \\ a_{24} & \dots & a_{14} & a_{13} \end{bmatrix} \begin{bmatrix} \Delta u(t_{-12}) \\ \Delta u(t_{-11}) \\ \vdots \\ \Delta u(t_{-1}) \end{bmatrix} \quad (5)$$

or

$$[y_p \text{ (future)}]_{12 \times 1} = [y(t_{-n_p})]_{12 \times 1} + [A_p]_{12 \times 12} [\Delta u \text{ (past)}]_{12 \times 1} \quad (6)$$

where

$$[A_p]_{12 \times 12} = \begin{bmatrix} a_{13} & \dots & a_3 & a_2 \\ a_{14} & \dots & a_4 & a_3 \\ \vdots & \dots & \vdots & \vdots \\ a_{24} & \dots & a_{14} & a_{13} \end{bmatrix}$$

where  $y(t_{-n_p})$  is the value of the process variable at the beginning of prediction  $n_p$  steps in the past. For a system at initial steady state, the process variables at the beginning of prediction during moving horizon control  $\{y(t_{-n_p}), y(t_{-n_p+1}), \dots, y(t_{-1})\}$  are all zero for  $t < t_0$ .

If the setpoint profile  $y_{sp}$  for  $t > t_0$  is known, we may define the free-response error vector as

$$\begin{bmatrix} E(t_1) \\ E(t_2) \\ \vdots \\ E(t_{12}) \end{bmatrix} = \begin{bmatrix} y_{sp}(t_1) \\ y_{sp}(t_2) \\ \vdots \\ y_{sp}(t_{12}) \end{bmatrix} - \begin{bmatrix} y_p(t_1) \\ y_p(t_2) \\ \vdots \\ y_p(t_{12}) \end{bmatrix} \quad (7)$$

or

$$[E]_{12 \times 1} = [y_{sp}]_{12 \times 1} - [y_p]_{12 \times 1} \quad (8)$$

To reduce or suppress the free-response error, DMC must instruct the final control element to make control moves for  $n_c$  steps at the present and future time steps ( $t_0, t_1, t_2, \dots, t_{nc-1}$ ).

#### Calculation of present and future control moves

If the controller makes control moves of  $\Delta u(t_0), \Delta u(t_1), \Delta u(t_2), \Delta u(t_3)$ , and  $\Delta u(t_4)$  for  $n_c$  steps (= 5 in this work), we may anticipate that such present and future control moves would cause the process to respond by the magnitudes given by Eqs. (3) and (4). Therefore, the free response error may be reduced due to the present and future control moves, resulting in an effective or net error expressed as a net error vector  $[NE]_{12 \times 1}$ :

*Net Error = (Free response error due to past control moves  $\Delta u(t < t_0)$ ) –*

*(Process response due to present and future control moves  $\Delta u(t \geq t_0)$ )*

$$\begin{bmatrix} NE(t_1) \\ NE(t_2) \\ \vdots \\ NE(t_{12}) \end{bmatrix} = \begin{bmatrix} E(t_1) \\ E(t_2) \\ \vdots \\ E(t_{12}) \end{bmatrix} - \begin{bmatrix} a_1 & 0 & \cdot & \cdot & 0 \\ a_2 & a_1 & 0 & \cdot & 0 \\ a_3 & a_2 & a_1 & 0 & 0 \\ \cdot & \cdot & \cdot & \cdot & \cdot \\ a_{11} & a_{10} & a_9 & a_8 & a_7 \\ a_{12} & a_{11} & a_{10} & a_9 & a_8 \end{bmatrix} \begin{bmatrix} \Delta u(t_0) \\ \Delta u(t_1) \\ \Delta u(t_2) \\ \Delta u(t_3) \\ \Delta u(t_4) \end{bmatrix} \quad (9)$$

$$[NE]_{12 \times 1} = [E]_{12 \times 1} - [A]_{12 \times 5} [\Delta u \text{ (present and future)}]_{5 \times 1} \quad (10)$$

It can be said that the present and future control moves would serve to reduce or suppress the free response error. In Eqs. (9) and (10), it is assumed that disturbance does not exist and that there is no mismatch between the measured and predicted process variable. It is also assumed that the controller does not reach saturation and there is no constraint on the control moves. To compute the present and future control moves, an objective function  $\Phi$  is defined as

$$\Phi = \sum_{i=1}^{n_p} \{ [NE(t_i)]^2 + \lambda [\Delta u(t_i)]^2 \} \quad (11)$$

where  $\lambda$  is defined as the move suppression coefficient.

***Moving horizon control is a key feature of dynamic matrix control. This type of controller employs a model internal to the controller architecture to predict the process variable for  $n_p$  steps into the future based on control moves for  $n_p$  steps in the past.***

Optimization of DMC gives the required present and future control moves that will serve to minimize  $\Phi$  for a given  $\lambda$ <sup>[1,3]</sup>

$$\Delta u \text{ (present and future)}]_{5 \times 1} =$$

$$\begin{bmatrix} \Delta u(t_0) \\ \Delta u(t_1) \\ \Delta u(t_2) \\ \Delta u(t_3) \\ \Delta u(t_4) \end{bmatrix} = ([A^T]_{5 \times 12} [A]_{12 \times 5} + \lambda [I]_{5 \times 5})^{-1} [A^T]_{5 \times 12} [E]_{12 \times 1} \quad (12)$$

where  $[A^T]$  is the transpose of the dynamic matrix  $[A]$  and  $[I]$  is a  $5 \times 5$  identity matrix for  $n_c = 5$ . Apparently, the greater the move suppression coefficient  $\lambda$ , the smaller the  $\Delta u(t_i)$  values or a more conservative control action; and vice versa the control action becomes more aggressive.

Once the calculation is done, only the first control move  $\Delta u(t_0)$  is implemented and the horizon moves one time step further. By treating  $t_1$  as the present time,  $t_0$  is then one time step in the past, and so forth. In the next step of calculation at  $t_1$ , the previously calculated  $\Delta u(t_0)$  would be considered as the control move one step in the past. So, its value (and only this  $\Delta u$ ) should be entered at the bottom of the  $[\Delta u(\text{past})]$  vector for the past control moves [second term on the right-hand side of Eqs. (5) and (6)]. Then  $[y_p]$ ,  $[E]$ ,  $[NE]$ , and the new  $[\Delta u(\text{present and future})]$  are recalculated at  $t_1$ . The whole procedure may be repeated for  $n_p$  steps.

If there is no mismatch between the measured and predicted process response, then the actual process response for future steps at  $t_1, t_2, \dots$  should be the sum of the free response and

the process response due to present and future moves [Eq. (13)]

$$y[(\text{actual response})]_{1 \times 1} = [y_p]_{1 \times 1} + [A]_{12 \times 5} [\Delta u(\text{present and future})]_{5 \times 1} \quad (13)$$

However, since only the first control move  $\Delta u(t_0)$  is implemented at  $t_0$ , we may predict the actual process response of  $y(t_1)$  only [Eq. (14)]

$$y(t_1) = y_p(t_1) (\text{predicted at } t_0 \text{ based on } y(t_{12}) \text{ and } [\Delta u(\text{past})]) + a_1 \Delta u(t_0) \quad (14)$$

*As the control horizon moves forward, the whole calculation repeats.*

As the control horizon moves forward, the whole calculation repeats. In a system where  $a_1 = 0$  (due to dead time), the actual process response  $y(t_1)$  is the same as the free response  $y_p(t_1)$  predicted at  $t_0$  due to past control moves.

### SAMPLE CALCULATION BY SPREADSHEET PROCEDURE

Based on the MPC theory and DMC strategy outlined above, the authors developed a spreadsheet procedure using data for a hypothetical first-order-plus-dead-time model with process gain  $K_p = 1.5$ , time constant  $\tau_p = 1$ , and deadtime  $\theta_p = 1$ . The SRM coefficients for this process model are shown in Table 1 and Figure 1. The size of time step  $\Delta t = 1$  is chosen in this work. This process stabilizes in 10 time steps or model horizon  $m = 10$ . The established DMC guidelines recommend that the pre-

**TABLE 1**  
Coefficient of step response model (SRM) used in this work

$a_1$	$a_2$	$a_3$	$a_4$	$a_5$	$a_6$	$a_7$	$a_8$	$a_9$	$a_{10}$
0.00	0.948	1.297	1.425	1.473	1.490	1.496	1.499	1.499	1.500
$a_{11}$	$a_{12}$	$a_{13}$	$a_{14}$	$a_{15}$	$a_{16}$	$a_{17}$	$a_{18}$	$a_{19}$	$a_{20}$
1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500
$a_{21}$	$a_{22}$	$a_{23}$	$a_{24}$	$a_{25}$	$a_{26}$	$a_{27}$	$a_{28}$	$a_{29}$	$a_{30}$
1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500

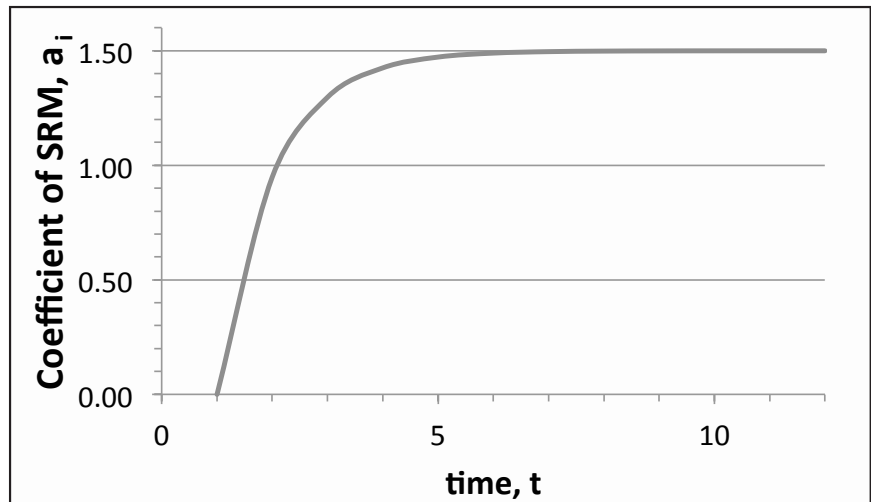


Figure 1. Plot of SRM Coefficient  $a_i$  versus time.

**TABLE 2**  
Dynamic matrix  $[A]_{12 \times 5}$  for prediction horizon  $n_p = 12$  and control horizon  $n_c = 5$  using the coefficients  $a_i$  ( $i = 1, 2, \dots, 12$ ) from the SRM.

0.000	0.000	0.000	0.000	0.000
0.948	0.000	0.000	0.000	0.000
1.297	0.948	0.000	0.000	0.000
1.425	1.297	0.948	0.000	0.000
1.473	1.425	1.297	0.948	0.000
1.490	1.473	1.425	1.297	0.948
1.496	1.490	1.473	1.425	1.297
1.499	1.496	1.490	1.473	1.425
1.499	1.499	1.496	1.490	1.473
1.500	1.499	1.499	1.496	1.490
1.500	1.500	1.499	1.499	1.496
1.500	1.500	1.500	1.499	1.499





**TABLE 5**

Calculation of  $[\Delta u \text{ (present and future)}]_{S_{k1}}$  to be carried out at  $t_0, t_1, \dots, t_4$  based on free response of process variable  $y_p(t_1, t_2, \dots, t_{12})$  and past  $\Delta u(t_{-12}, t_{-11}, \dots, t_{-1})$ . Note that only the first of the present and future  $\Delta u$  (0.410) is actually carried out at  $t_0$ .

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R
62									y @ t <sub>1</sub>									
63				t	0	count, now & past	count, now & future	-12	$\Delta u$ (past)	[A <sub>p</sub> ] [ $\Delta u$ (past)]	y <sub>p</sub> (free response)	y <sub>sp</sub>	[E]	$\Delta u$ (now & future)	y(next)	y(now & past)		
64						=I65 & copied downwards	0	=Q65			=I65+K65		=M65-L65	0.410	=L65+O64*SE\$7			
65							-12	1	0.000	0.000	0.000	1.000	1.000	0.176	0.000	0.000		
66							-11	2	0.000	0.000	0.000	1.000	1.000	0.064		0.000		
67							-10	3	0.000	0.000	0.000	1.000	1.000	0.018		0.000		
68							-9	4	0.000	0.000	0.000	1.000	1.000	0.001		0.000		
69							-8	5	0.000	0.000	0.000	1.000	1.000			0.000		
70							-7	6	0.000	0.000	0.000	1.000	1.000	=MMULT(\$E\$28:\$P\$32, N65:N76)		0.000		
71							-6	7	0.000	0.000	0.000	1.000	1.000			0.000		
72							-5	8	0.000	0.000	0.000	1.000	1.000			0.000		
73							-4	9	0.000	0.000	0.000	1.000	1.000			0.000		
74							-3	10	0.000	0.000	0.000	1.000	1.000			0.000		
75							-2	11	0.000	0.000	0.000	1.000	1.000			0.000		
76							-1	12	0.000	0.000	0.000	1.000	1.000			0.000		
77							0		0.410							0.000		
78									=O64		=MMULT(\$E\$37:\$P\$48, I65:J76)							

**TABLE 6**

Calculation of  $\Delta u$  to be carried out at  $t_1, t_2, \dots, t_5$  based on predicted process variable  $y_p(t_2, t_3, \dots, t_{13})$  and past  $\Delta u(t_{-11}, t_{-3}, \dots, t_0)$ . Only the first of the present and future  $\Delta u$  (0.176) is actually carried out at  $t_1$ . Important cell operations are explained in the text.

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R
79				t	1	count, now & past	count, now & future	=I63+1	-11	$\Delta u$ (past)	[A <sub>p</sub> ] [ $\Delta u$ (past)]	y <sub>p</sub> (free response)	y <sub>sp</sub>	[E]	$\Delta u$ (now & future)	y(next)	y(now & past)	
80																		
81							=I63+1	1	=Q82						0.176			
82							-11	2	0.000	0.000	0.389	0.389	1.000	0.611	0.064	0.389	0.000	
83							=G65+1	-10	3	0.000	0.000	0.532	0.532	1.000	0.468	0.018	0.000	
84								-9	4	0.000	0.000	0.585	0.585	1.000	0.415	0.002	0.000	
85								-8	5	0.000	0.000	0.604	0.604	1.000	0.396	-0.002	0.000	
86							=I82	-7	6	0.000	0.000	0.611	0.611	1.000	0.389		0.000	
87								-6	7	0.000	0.000	0.614	0.614	1.000	0.386		0.000	
88								-5	8	0.000	0.000	0.615	0.615	1.000	0.385		0.000	
89								-4	9	0.000	0.000	0.615	0.615	1.000	0.385		0.000	
90								-3	10	0.000	0.000	0.615	0.615	1.000	0.385		0.000	
91								-2	11	0.000	0.000	0.615	0.615	1.000	0.385		0.000	
92								-1	12	0.000	0.000	0.615	0.615	1.000	0.385		0.000	
93								0	13	0.000	0.410	0.615	0.615	1.000	0.385		0.000	
94								1		0.176						=Q77 and copied upwards	0.000	
95										=O81	=J77 (and copied upwards)					=P65		

- (8) Highlight cell O64-O68 and perform matrix multiplication according to Eq. (12), where the  $[A^T][A] + \lambda [I]$  ( $A^T$ ) (for  $\lambda=3.0$ ) is given in Table 3. Again, in the matrix multiplication “=MMULT(\$E\$28:\$P\$32, N65:N76),” E28-P32 is the matrix  $[A^T][A] + \lambda [I]$  and its column number and row number must be fixed by placing the \$ sign in front of them. However, the cell positions in the [E] vector do not need the \$ sign. The cells O64-O68 are the predicted control moves to be made at  $t_0, t_1, \dots, t_4$ . But only the first one (O64, with calculated value of 0.410) will be actually implemented;
- (9) Highlight cell J77 and assign “= O64.” In this way, the present  $\Delta u(t_0)$  is entered to the bottom of Column J;
- (10) Highlight cell P65 to calculate the actual process variable  $y(\text{next})$  or  $y(t_1)$  according to Eq. (14) to show the effect of the present control move  $\Delta u(t_0)$ . In the au-

thors’ spreadsheet, the coefficient of SRM  $a_1$  is located at cell E7.

To perform the calculation for the moving horizon control, the cells in Table 5 are copied and pasted somewhere else on the spreadsheet for calculations at the next time step at  $t_1$ . The pasted cell needs revision before the final outcome (Table 6) is obtained:

- (1) Highlight the cell G82 and perform “= G65 + 1” and copy downward. The count for now and past will be advanced by 1 from corresponding cells of Table 5. Do the same for H81-H93 and cell I80;
- (2) Highlight Q94 and perform “= P65.” Doing so will put the  $y(\text{next})$  calculated at  $t_0$  as the value of the process valuable  $y(\text{now})$  at  $t_1$ ;
- (3) Highlight Q93, perform “= Q77,” and copy the formula upward. In this manner, the process vari-

**TABLE 7**

Calculation of  $[\Delta u(\text{present and future})]$  to be carried out at  $t_2, t_3, \dots, t_6$  based on predicted process variable  $y_p(t_3, t_4, \dots, t_{14})$  and past  $\Delta u(t_{10}, t_9, \dots, t_1)$ . This section is the result of copying the cells in Table 6 and pasting it somewhere below.

	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R
96						y @ t									
97	t	2.000		count, now & past	count, now & future	-10.000	$\Delta u(\text{past})$	$[A_p]$ [ $\Delta u(\text{past})$ ]	$y_p$ (free response)	$y_{sp}$	[E]	$\Delta u(\text{now}$ & future)	y(next)	now & past	
98					2							0.064			
99				-10	3	0.000	0.000	0.699	0.699	1.000	0.301	0.018	0.699	0.000	
100				-9	4	0.000	0.000	0.813	0.813	1.000	0.187	0.003		0.000	
101				-8	5	0.000	0.000	0.855	0.855	1.000	0.145	-0.002		0.000	
102				-7	6	0.000	0.000	0.870	0.870	1.000	0.130	-0.002		0.000	
103				-6	7	0.000	0.000	0.876	0.876	1.000	0.124			0.000	
104				-5	8	0.000	0.000	0.878	0.878	1.000	0.122			0.000	
105				-4	9	0.000	0.000	0.879	0.879	1.000	0.121			0.000	
106				-3	10	0.000	0.000	0.879	0.879	1.000	0.121			0.000	
107				-2	11	0.000	0.000	0.879	0.879	1.000	0.121			0.000	
108				-1	12	0.000	0.000	0.879	0.879	1.000	0.121			0.000	
109				0	13	0.000	0.410	0.879	0.879	1.000	0.121			0.000	
110				1	14	0.000	0.176	0.879	0.879	1.000	0.121			0.000	
111				2			0.064							0.389	
112															
113						y @ t									
				count, now & past	count, now & future			$[A_p]$	$y_p$ (free response)	$y_{sp}$	[E]	$\Delta u(\text{now}$ & future)			

**TABLE 8**

Results for  $t = 12$ . Additional column S267-S281 displays the cumulative controller output  $u$ .

	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S
263				10	23	0.000	0.000	1.000	1.000	1.000	0.000			1.001		
264				11			0.000							1.000		
265																
266						y @ t										
267	t	12.000		count, now & past	count, now & future	0.000	$\Delta u(\text{past})$	$[A_p]$ [ $\Delta u(\text{past})$ ]	$y_p$ (free response)	$y_{sp}$	[E]	$\Delta u(\text{now}$ & future)	y(next)	now & past		u
268					12							0.000				=S268+J269
269				0	13	0.000	0.410	1.000	1.000	1.000	0.000	0.000	1.000	0.000	and copied downwards	0.410
270				1	14	0.000	0.176	1.000	1.000	1.000	0.000	0.000	0.000			0.586
271				2	15	0.000	0.064	1.000	1.000	1.000	0.000	0.000	0.000			0.650
272				3	16	0.000	0.018	1.000	1.000	1.000	0.000	0.000	0.699			0.668
273				4	17	0.000	0.003	1.000	1.000	1.000	0.000	0.000	0.874			0.671
274				5	18	0.000	-0.001	1.000	1.000	1.000	0.000	0.000	0.955			0.670
275				6	19	0.000	-0.001	1.000	1.000	1.000	0.000	0.000	0.988			0.668
276				7	20	0.000	-0.001	1.000	1.000	1.000	0.000	0.000	0.999			0.667
277				8	21	0.000	0.000	1.000	1.000	1.000	0.000	0.000	1.001			0.667
278				9	22	0.000	0.000	1.000	1.000	1.000	0.000	0.000	1.001			0.667
279				10	23	0.000	0.000	1.000	1.000	1.000	0.000	0.000	1.001			0.667
280				11	24	0.000	0.000	1.000	1.000	1.000	0.000	0.000	1.000			0.667
281				12			0.000						1.000			0.667
282																
283																

able calculated in the time step before will move up one position;

- (4) Highlight J93, perform “= J77” (the bottom of J column in Table 5), and copy the formula upward. In this manner, the  $\Delta u(\text{past})$  from the previous table will move up by one position;
- (5) The users will then see the revised result of cells O81-O85. Finally, Highlight J94 and perform “= O81” to enter the present control move just calculated.

Once Table 5 and Table 6 are established, the content of Table 6 can be copied and pasted somewhere down below without any further revisions because the relationships between two successive tables are already established. The result of calculations at  $t_2$  is given in Table 7. If the contents of Table 6 are pasted for subsequent time steps, the final results of calculations for  $t_{12}$  are shown in Table 8. In Table 8, the cell S269 is highlighted and “= S268+J269” is performed and copied downward. In this way, the cumulative controller output may be calculated from the control moves since  $t_0$  (Column J).

Figure 2 shows the process response ( $y$ ), control moves at every time step ( $\Delta u$ ), cumulative controller output ( $u$ ) and setpoint ( $y_{\text{setpoint}}$ ) for time steps up to  $n_p = 12$  (Table 8). Once the calculations are done for  $\lambda = 3$ , the contents of this worksheet may be copied and pasted on several other worksheets. By simply changing the cell that stores the  $\lambda$  value, the results for  $\lambda = 1, 5, 8$ , and  $20$  would appear immediately. Figures 3 and 4 summarize the effects of moving suppression coefficient  $\lambda$  on the process variable  $y$  as well as cumulative controller output  $u$ . It is clear that the greater the  $\lambda$  value, the more conservative the control action and the more sluggish in process response.

## DISCUSSION

This work focuses on setpoint tracking in the absence of disturbance for perfectly linear process models. In reality, many real-world processes exhibit non-linear behaviors, with SRM coefficients ( $a_i$ 's) varying with steady-state conditions. Also, it is assumed that there is no process or model mismatch between the predicted and measured values of process variable at  $t_0$ . If such a mismatch exists, the magnitude  $\varepsilon = y_{\text{sp}}(t_0) - y_p(t_0)$  must be subtracted from every element of the vector  $[E]$  in Eqs. (7) and (8) to make the prediction more accurate.

With the model having the first-order-plus-dead-time behavior, there are many well-established tuning rules available to tune the feedback controller for this process. However, DMC offers several benefits. DMC is able to predict the future errors and the present and future control moves in order to minimize predicted net errors for future steps. This ability of changing controller outputs based on the predicted future process condition is absent in traditional feedback control. Or, we may say that a DMC system having a very short prediction horizon ( $n_p$ ) behaves more like a traditional feedback controller. In this work, the authors choose  $n_p$ ,  $m$ , and  $n_c$  according to recommended guidelines. Because the control action cannot change after the control horizon ends, a short control horizon  $n_c$  results in a large initial controller output, but a few careful changes in control action. The large control action in a short control horizon might overshoot the setpoint. However, as the controller continues to execute, the process variable will eventually settle around setpoint. On the other hand, a long control horizon produces a small initial controller output but more aggressive changes in control action. These aggressive changes in control action in a long control horizon can result in oscillation. In general, a control horizon of about one-half model horizon is recommended. Although a long prediction horizon increases the predictive ability of the DMC, the performance of the controller may suffer due to the extra calculations required.

The spreadsheet procedure developed here allows students to track step-by-step changes of a moving horizon control system with great ease. Interested users may revise this spreadsheet by

- (1) using SRM coefficients obtained from real-world

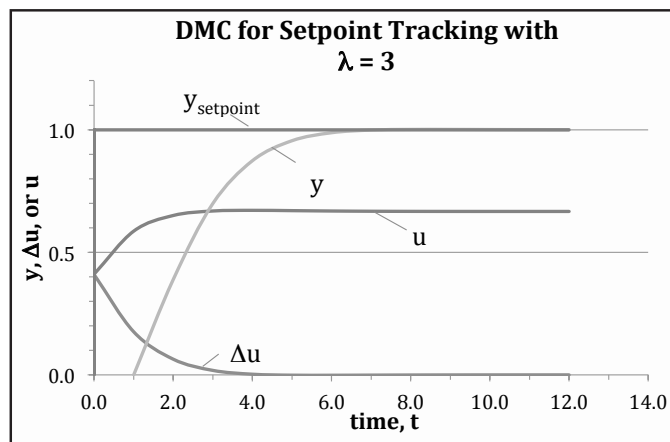


Figure 2. Results of calculation for setpoint tracking by DMC with move suppression coefficient  $\lambda = 3$ . Since  $a_1 = 0$  in this case,  $y = y_p$ .

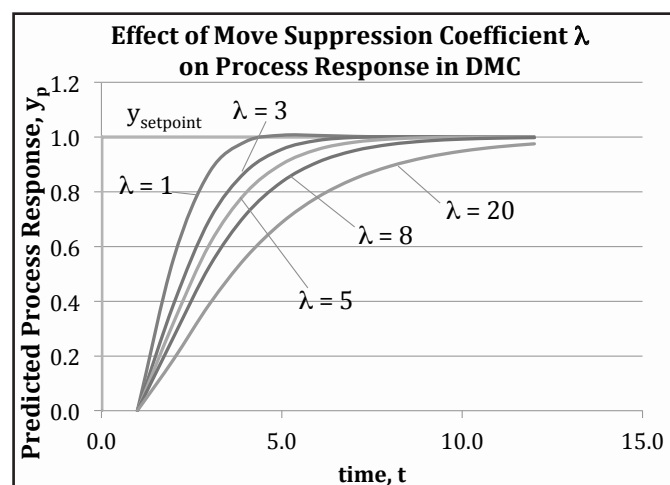


Figure 3. Effect of move suppression coefficient  $\lambda$  on the actual process response  $y$  or free response  $y_p$ , same for this case with  $a_1 = 0$ .

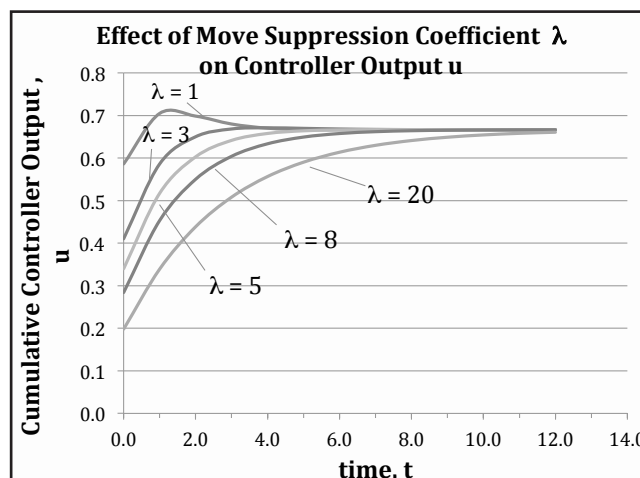


Figure 4. Effect of move suppression coefficient  $\lambda$  on the controller output  $u$ .



processes or real plant data;

- (2) removing or changing the amount of dead time to explore the effects of dead time on  $y$  and  $u$ . In the absence of dead time, the free response  $y_p(\text{next})$  and actual response  $y(\text{next})$  will differ by a magnitude of  $a_1^* \Delta u(\text{present})$ , where  $a_1 \neq 0$ ;
- (3) consulting with publications that use more sophisticated software<sup>(4)</sup> once they are confident in the basic concept; or
- (4) exploring the effects of using different values for various horizons (model horizon, prediction horizon, and control horizon).

The topic of DMC was covered in our department's process control class for the first time in the Fall 2014 semester, as suggested by our department's industrial associates. The topics covered in this class are listed below:

- Introduction to the course, control practice, elements of typical control systems, design of data acquisition using modern software such as LabVIEW
- Case study of process dynamic model: heated stirred tank—from energy balance to closed-loop control system, and case studies including laboratory control experiments
- Derivation of dynamic models for industrially important process units
- Review of essential mathematical tools (differential equations and Laplace Transform)
- Dynamic behavior of first-order systems (first experience of Loop Pro software); Dynamic Matrix
- Dynamic behavior of second-order systems
- Higher order systems and approximate models for poorly understood systems
- Overall transfer function of closed-loop feedback control systems
- Stability analysis
- Process identification of typical chemical engineering processes
- Industrial procedure of controller tuning (process reaction curve method, continuous cyclic response method, frequency response method)
- Industrial procedure of controller tuning (Internal Model Control (IMC))
- Advanced Control Methods—Cascade, Feedforward/Feedback, Smith Predictor, Gain Scheduling
- Introduction to Dynamic Matrix Control

Besides two hours of lecture each week, this course has a Laboratory/Problem (L/P) component that meets three hours each week. During the L/P hours, students have opportunities running real-world experiments, performing simulation using Loop-Pro software (Workshop 1 through 3 below), and designing spreadsheet procedures (Workshop 4):

- **Workshop #1:** Level control in gravity drained tanks
- **Workshop #2:** Temperature control in shell-n-Tube heat exchangers
- **Workshop #3:** Level control in pumped tanks
- **Workshop #4:** Spreadsheet procedure for Dynamic Matrix Control calculations

Although the topic of DMC and the associated spreadsheet workshop were covered toward the end of the semester for one lecture and one L/P activity, students had a chance to learn the basics of this advanced concept.

## CONCLUSIONS

1. An easy-to-follow spreadsheet procedure is developed for an undergraduate process control class to learn basic aspects of moving horizon control in a dynamic matrix controller (DMC);

2. Based on coefficients of step response model (SRM) obtained from plant data, a dynamic matrix can be constructed for a DMC;

3. The DMC calculates the present and future control moves required to decrease the predicted future errors (and steer the process variable toward setpoint) according to the rules of DMC and a selected value of move suppression coefficient  $\lambda$ ; and

4. The greater (smaller) the  $\lambda$  value, the more conservative (aggressive) the control action.

## ACKNOWLEDGMENT

This work is partially supported by Faculty Sabbatical Leave Award (Jang) and Research, Scholarship, and Creative Activity Award (Lo) from California State University, Long Beach.

## REFERENCES

1. Riggs, J.B., and M.N. Karim, *Chemical and Bio-Process Control*, 3rd Ed. Lubbock, Tex.: Ferret Pub, 2007
2. Lee, J.H., "Model Predictive Control: Review of the Three Decades of Development," *Int. J. Control Autom. Syst.*, **9**(3), 415, (2011)
3. Camacho, E., and C. Bordons, *Model Predictive Control*, 1st Ed. Berlin; New York: Springer, 1999
4. Wang, L., *Model Predictive Control System Design and Implementation Using MATLAB®*, Springer Science & Business Media, 2009 □